

On the role of the bed-load thickness in the dune instability mechanisms

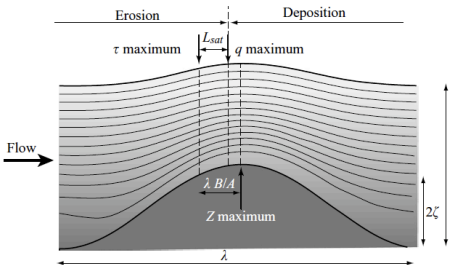
and how numerical simulation could help ...

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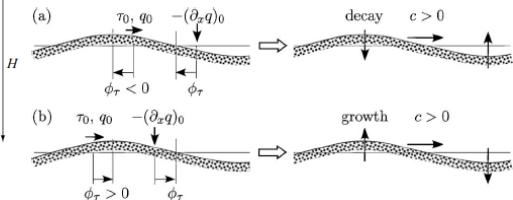
Atelier Fluide OSUG

18th june 2012



Fourriere et al., JFM (2010)

Charru, PoF (2006)



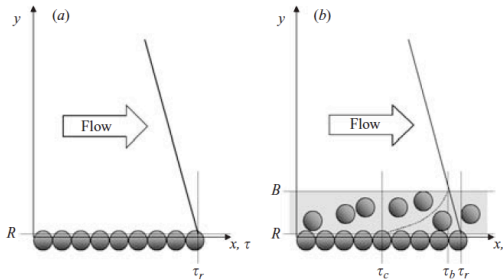
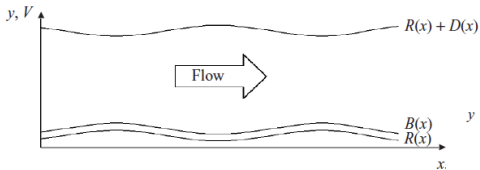
Destabilising mechanisms:

→ Phase shift between the bed shear stress and the topography due to fluid inertia
eg. Kennedy, JFM (1963); Ouriemi et al. JFM (2009)

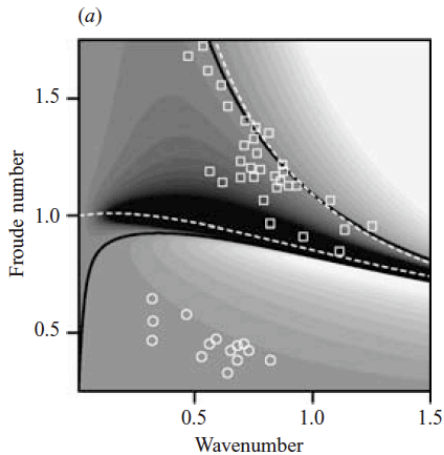
Stabilising mechanisms:

- Gravity *e.g. Kennedy, JFM (1963)*
- Bed-load thickness *Colombini, JFM (2004)*
- Saturation length *Fourriere et al., JFM (2010)*
- Free surface *Fourriere et al., JFM (2010)*
- Suspended load *Engelund and Fredsoe, ARFM (1974)*

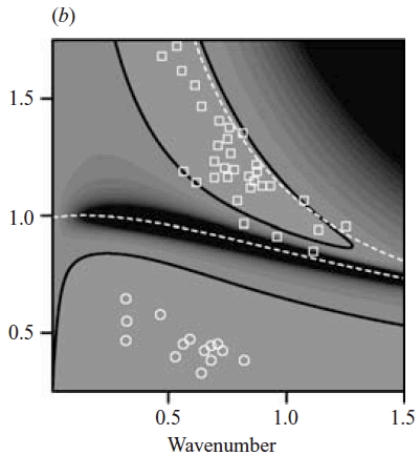
⇒ **No clear picture of bedforms formation !!!**



... the *phaselag between sediment transport and bed elevation* remains the *main mechanism driving instability*. However, it is shown that this phase-lag varies significantly in a neighbourhood of the bed. Moreover, since the *layer in which sediments are moving has a finite (though small) thickness*, it is assumed that the perturbations of the *fluid stress driving bedload transport* should be *evaluated at the top of the layer itself*. It is shown that such an apparently minor modification of the classical approach *alters remarkably the balance between stabilizing and destabilizing effects that drives the instability process*.



Bed-load thickness = 0



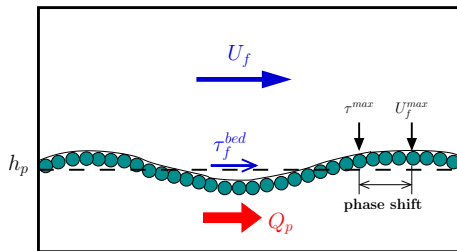
Empirical bed-load thickness

Growth rate plot ; experiments of Guy et al. (1966): \circ dunes; \square , antidunes.

Dark color = Stable; Thick solid lines = marginal curves

Colombini, JFM (2004)

Particle Flux



Navier-Stokes

+

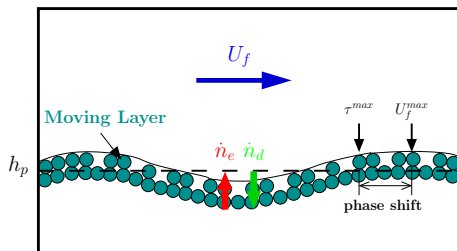
Mass conservation

$$\phi \frac{\partial h_p}{\partial t} + \frac{\partial Q_p(\theta)}{\partial x} = 0$$

$$\rightarrow \theta = \frac{\tau_f^{bed}}{\Delta \rho g d} : \text{Shields Number}$$

[Engelund and Fredsoe, 1982,
Richards, 1980, Colombini, 2004],...

Erosion / Deposition



Navier-Stokes

+

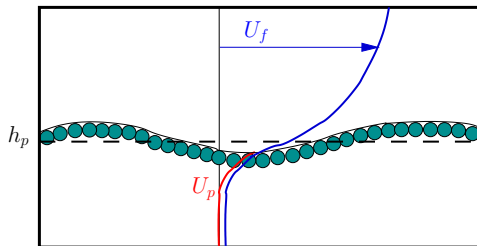
Mobile particle number conservation

$$\frac{\partial n}{\partial t} = \dot{n}_e - \dot{n}_d - \frac{\partial n u}{\partial x}$$

$$\rightarrow \dot{n}_e, \dot{n}_d : \text{Erosion / Deposition rate}$$

[Charru et al., 2004, Charru, 2006], ...

Two-phase model for bed-load transport in laminar flows



Navier-Stokes

+

→ *Mass conservation equation*

→ *Momentum equation*

Fluid + Particles

Closures :

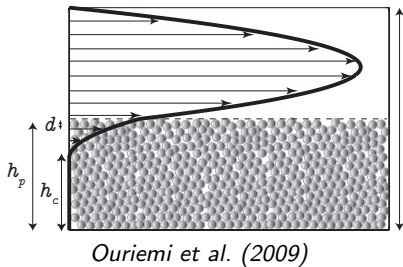
- Fluid: Newtonian rheology - Einstein's viscosity → $\eta_e = \eta_f (1 + 5/2 \phi)$
- Particles: Frictional rheology - Coulomb or $\mu(I)$ → $\tau^p = \mu p^p$
- Fluid-particles interaction : Buoyancy + Darcy → $\phi \vec{\nabla} \tau^f + \frac{\eta_f \epsilon^2}{K} (\vec{u}^f - \vec{u}^p)$

Set of equations to be solved

- Darcy-Brinkman for the fluid (Darcy dominant)
- Mixture momentum equation (Fluid+Particles)

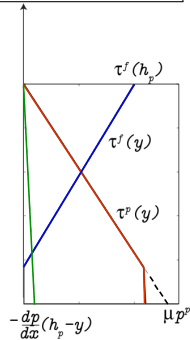
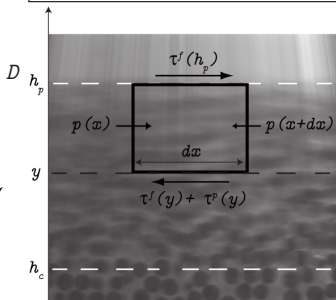
Ouriemi, Aussillous and Guazzelli, JFM (2009)

Analytical solution (Coulomb)



Mixture momentum balance

$$\tau^m(y) = \tau^p(y) + \tau^f(y) = \tau^f(h_p) - \frac{\partial p^f}{\partial x} (h_p - y)$$



Particle shear stress: Coulomb $\tau^p \leq \mu_s p^p = \mu_s \phi_0 \Delta \rho g (h_p - y)$ where p^p is hydrostatic

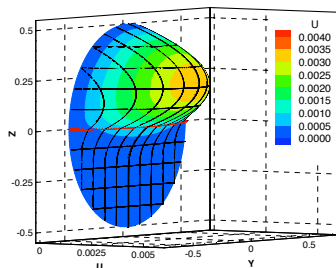
Fluid shear stress: $\tau^f = \eta_e \frac{\partial u^f}{\partial y}$

Velocity profile: $u^p \approx u^f \approx \frac{(\mu \phi_0 \Delta \rho g + \frac{\partial p^f}{\partial x}) (y - h_c)^2}{\eta_e} \Rightarrow q_p \text{ and } q_f \propto \boxed{q_0 = \Delta \rho g h_f^3 / \eta}$

Eulerian model \rightarrow **No influence of the particle size!** Shields number θ not the right parameter

Initial numerical model (Médale)

- ▶ 3D Navier-Stokes equations
- ▶ Finite Element Method
 - ▶ Velocity: Quadratic elements
 - ▶ Pressure: Linear elements
- ▶ Newton-Raphson algorithm



Non-dimensionalisation [Ouriemi et al., 2009]

Length: H ; Pressure: $\Delta\rho g H$; Time: $\eta_f / \Delta\rho g H$

3D two-phase numerical model (Chauchat & Médale, 2010)

1. Mixed-fluid model: mixture momentum equation \Rightarrow single effective phase
2. Two-fluid model: fluid and particle momentum equations

Issues

- ▶ Modeling friction (regularization)
- ▶ Coupled problem (fluid-particle interaction)

$$U_0 = \Delta\rho gh_f^2/\eta_f$$

— Coulomb 2D, — $\mu(I)$ 2D, - - $\mu(I)$ 3D

Borosilicate (d=1 mm)

$$Q_f = 3.58 \cdot 10^{-6} \text{ m}^3/\text{s}$$

(a)

Borosilicate (d=1 mm)

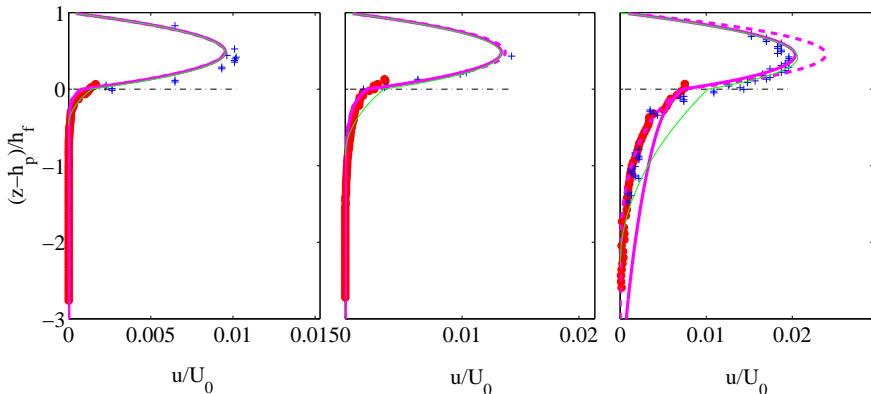
$$Q_f = 5.25 \cdot 10^{-6} \text{ m}^3/\text{s}$$

(b)

PMMA (d=2 mm)

$$Q_f = 1.23 \cdot 10^{-6} \text{ m}^3/\text{s}$$

(c)



→ 3D two-phase numerical model (Chauchat & Médale, CMAME 2010)

Aussillous *et al.*, submitted to JFM

Conclusion

- Continuous model for bed-load transport
- Phenomenological rheology used to describe intergranular stresses $\mu(I)/\phi(I)$
- 3D numerical model

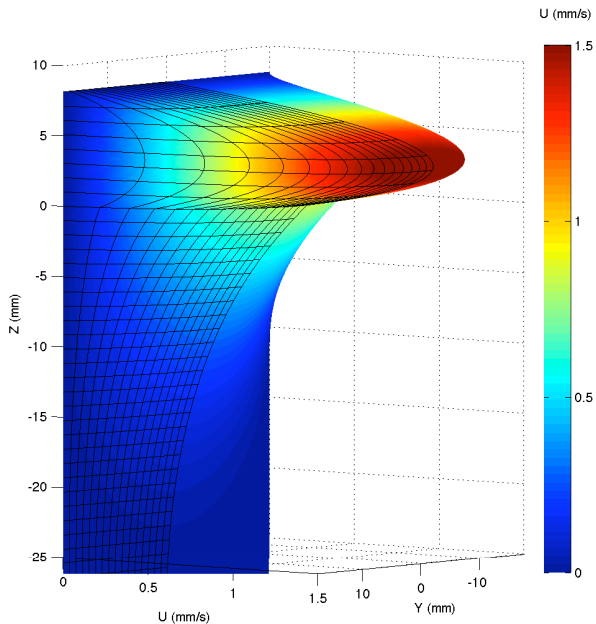
Perspectives

- Study numerically bedforms formation

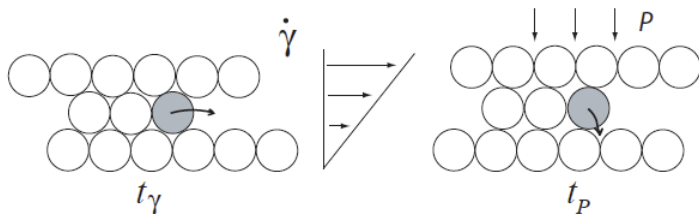
Collaborations

- ▶ IUSTI (Marseille) : P. Aussillous, E. Guazzelli, M. Médale
- ▶ LEGI (Grenoble) : E. Barthélémy, D. Hurther, H. Michallet, T. Revil-Baudard
- ▶ Univ. Savoie (Chambéry) : M. Pailha

3D velocity profile



Frictional rheology: the viscous regime



Andreotti, Forterre and Pouliquen (2011)

Interpretation of the Viscous number:

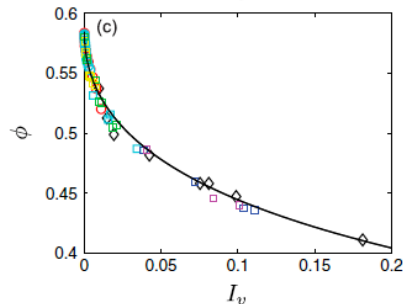
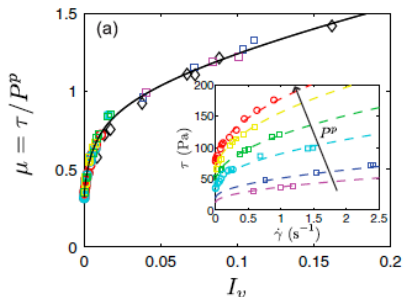
$$I_v = \frac{\dot{\gamma} \eta_f}{\alpha p^p} = \frac{t_{micro}}{t_{macro}} \quad \text{where} \quad t_{micro} = \frac{\eta_f}{\alpha p^p} \quad \text{and} \quad t_{macro} = \frac{1}{\dot{\gamma}}$$

Cassar, Nicolas and Pouliquen (2005), Boyer, Guazzelli and Pouliquen (2011)

The shear stress is proportional to the pressure and depends on I_v , also the volume fraction depends on I_v :

$$\tau = \mu(I_v) p^p \quad \text{and} \quad \phi = \phi(I_v)$$

Granular rheology for dense suspension

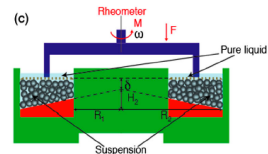
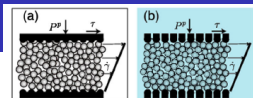


Two contributions:

$$\mu(I_v) = \mu^c + \mu^h$$

$\mu^c \rightarrow$ contact

$\mu^h \rightarrow$ hydrodynamic



Effective viscosity:

$$\mu^h(I_v) \Rightarrow \frac{\eta_e(\phi)}{\eta_f} = 1 + \frac{5}{2} \phi \left(1 - \frac{\phi}{\phi_m}\right)^{-1}$$

Friction coefficient:

$$\mu^c(I_v) = \mu_s + \frac{\mu_2 - \mu_s}{I_0/I_v + 1}$$

Volume fraction:

$$\phi(I_v) = \frac{\phi_m}{1 + I_v^{1/2}}$$

where $\phi_m = 0.585$, $\mu_s = 0.32$, $\mu_2 = 0.7$
and $I_0 = 0.005$

Boyer, Guazzelli and Pouliquen (2011)

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Selection of the ripple length on a granular bed sheared by a liquid flow.
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Erosion and deposition of particles on a bed sheared by a viscous flow.
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- [Colombini, 2004] Colombini, M. (2004).
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Journal of Fluid Mechanics, 502(-1):1–16.
- [Engelund and Fredsoe, 1982] Engelund, F. and Fredsoe, J. (1982).
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